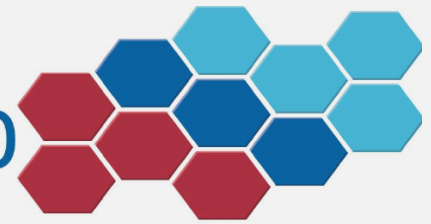




TECHNISCHE UNIVERSITÄT  
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SFB 920



Multifunktionale Filter für die Metallschmelzefiltration –  
ein Beitrag zu Zero Defect Materials

# Application of the discrete phase model in metallurgical processes

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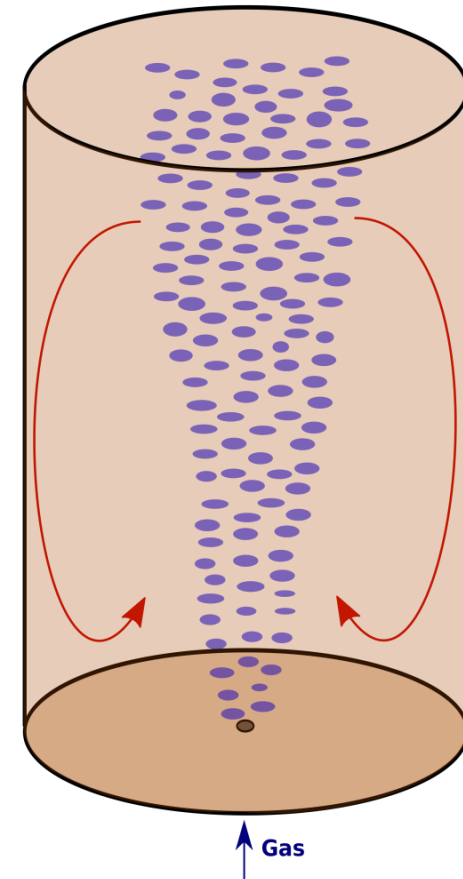


# Outline

- ❖ Motivation
- ❖ Discrete phase model
- ❖ Model validation
- ❖ Application in metallurgy
- ❖ Outlook

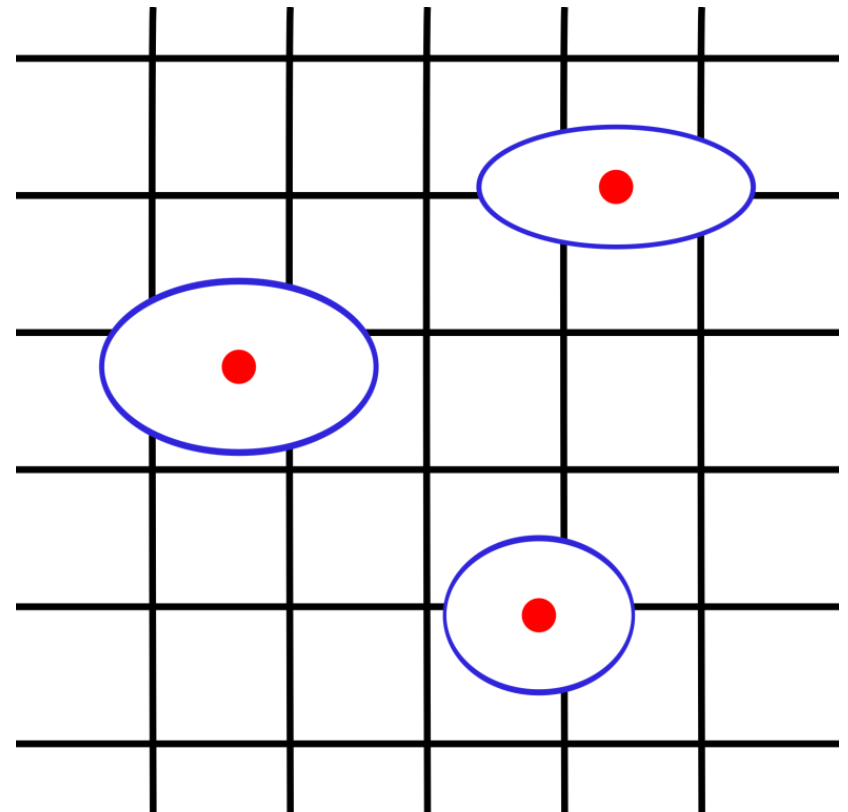
# Motivation

- a) Multi-phase flow of interest in metallurgical processes
- b) Bubbles/particles/slag/melt
- c) Considerable impact on flow pattern
- d) Detailed knowledge of interplay between phases to enhance steel quality
- e) Magnetic field used to control the melt flow



# Discrete phase model (DPM)

- a) Liquid as continuum
- b) Disperse phase in Lagrangian-way
- c) Disperse phase as mass point
- d) Bubbles or solid particles
- e) Without transient shape deformation
- f) Two-way coupling



# Discrete phase model (DPM)

## Equations in OpenFoam

### Navier-Stokes-Equation- NSG

$$\rho \frac{\partial \bar{u}}{\partial t} + \rho \bar{u} \cdot \nabla \bar{u} = -\nabla \bar{p} + \eta \Delta \bar{u} + \bar{f}_W + \bar{f}_L - \nabla \cdot \bar{\tau}^{RS}$$

$$\nabla \cdot \bar{u} = 0$$

Two-way coupling

One-way coupling

### Euler-Lagrange - EL

$$m_p \frac{du_p}{dt} = \underline{F}_B + \underline{F}_D + \underline{F}_{VM} + \underline{F}_{lift} + \underline{F}_G + \underline{F}_{press}$$

### Volume of Fluid - VOF

$$\frac{\partial \alpha}{\partial t} + \nabla \cdot (\underline{u} \alpha) + \nabla \cdot (\underline{u}_r \alpha (1 - \alpha)) = 0$$

### MHD

$$\bar{f}_L = \bar{j} \times \underline{B}_0$$

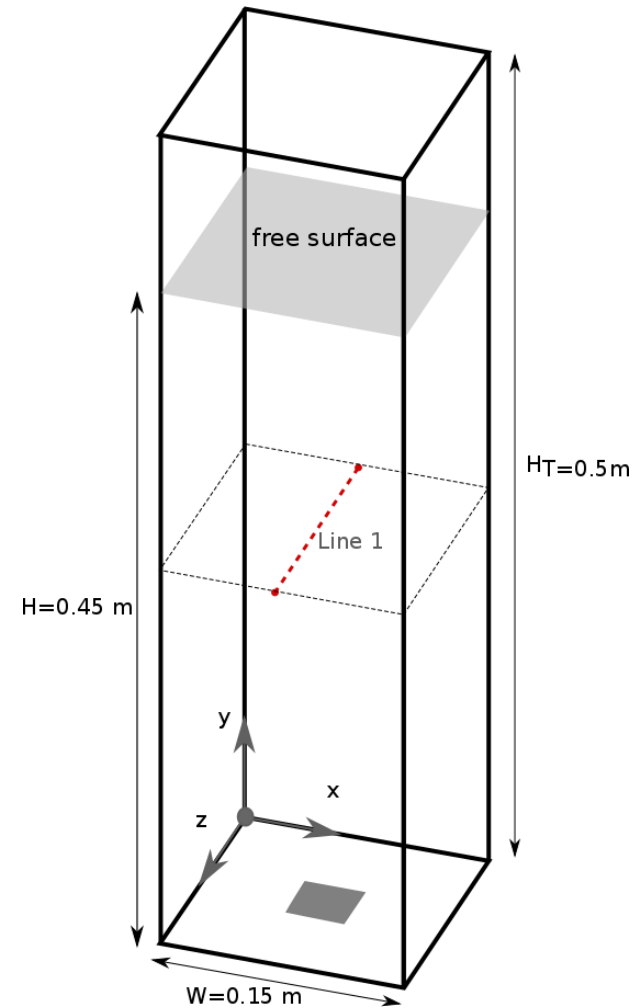
$$\bar{j} = \sigma (-\nabla \bar{\psi} + \bar{u} \times \underline{B}_0)$$

$$\nabla^2 \bar{\psi} = \nabla \cdot (\bar{u} \times \underline{B}_0)$$

Turbulence:  
LES/RANS or URANS

## Bubble column

- Experiment by Deen et al. [1]
- Water/air bubbles
- Sparger with 47 holes
- 3200 bubbles/second
- Bubble diameter 4 mm
- VOF to capture free surface
- DDES model
- Forces:  $\underline{F}_G, \underline{F}_B, \underline{F}_D, \underline{F}_{VM}, \underline{F}_L, \underline{F}_p$
- Comparison between drag models



# Model Validation

## Drag coefficient

a) Tomiyama drag model [2]

$$CD = \max \left\{ \min \left[ \frac{16}{Re_b} (1 + 0.15 Re_b^{0.687}), \frac{48}{Re_b} \right], \frac{8}{3} \frac{Eo}{Eo + 4} \right\}$$

b) Ishii and Zuber [3]

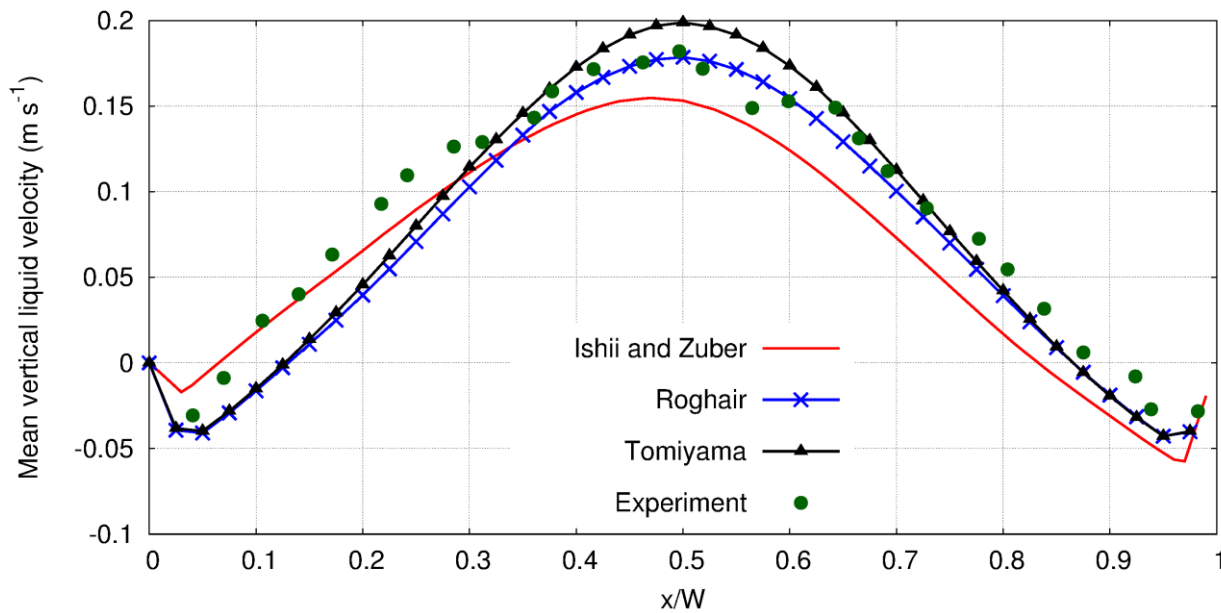
$$CD = \max \left\{ \frac{24}{Re_b} (1 + 0.15 Re_b^{0.687}), \min \left[ \frac{4}{3} \sqrt{2Eo}, \frac{8}{3} \right] \right\}$$

c) Roghair drag model [4]

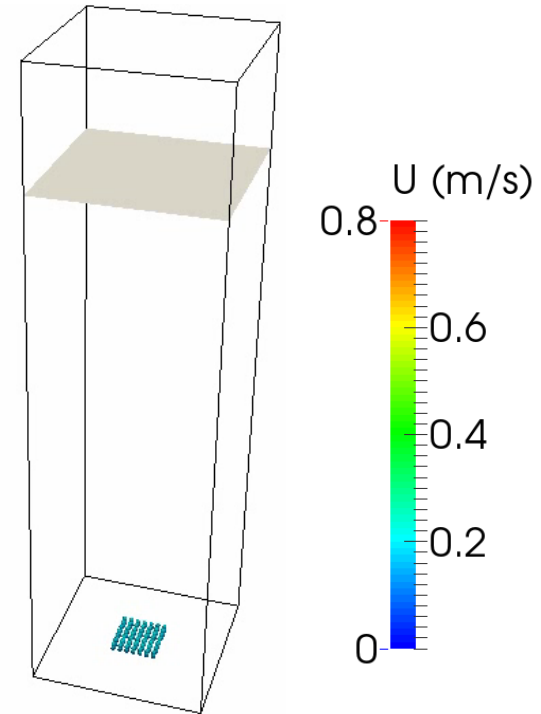
$$\frac{CD}{CD_\infty (1 - \alpha_{loc})} = f(Eo, \alpha_{loc}) = 1 + \left( \frac{18}{Eo} \right) \alpha_{loc}$$

$$CD_\infty = \sqrt{Cd(Re_b)^2 + Cd(Eo)^2}$$

## Results



Vertical velocity of liquid



3d View

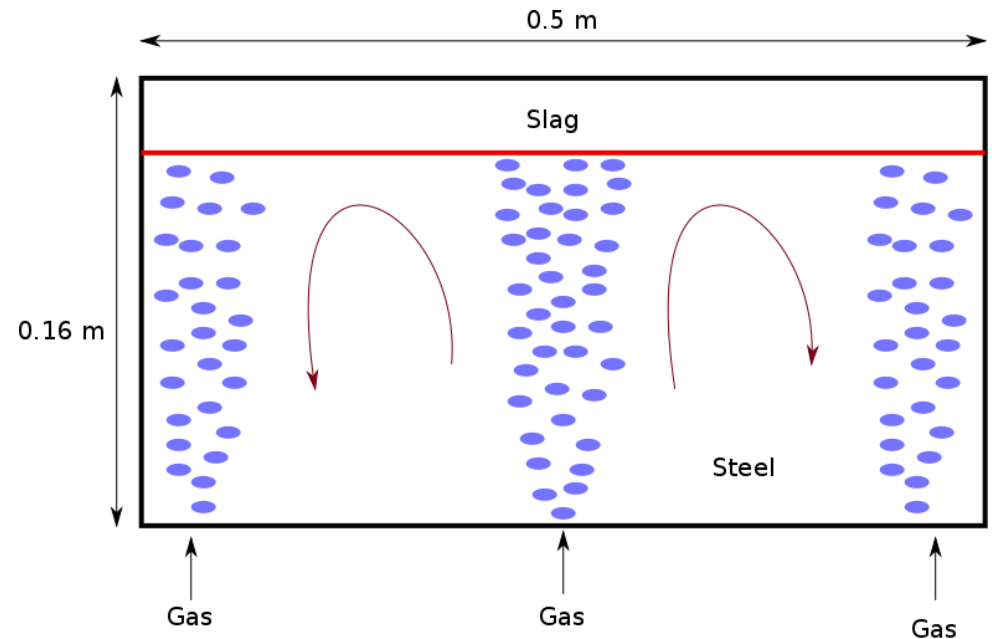


# Conclusion

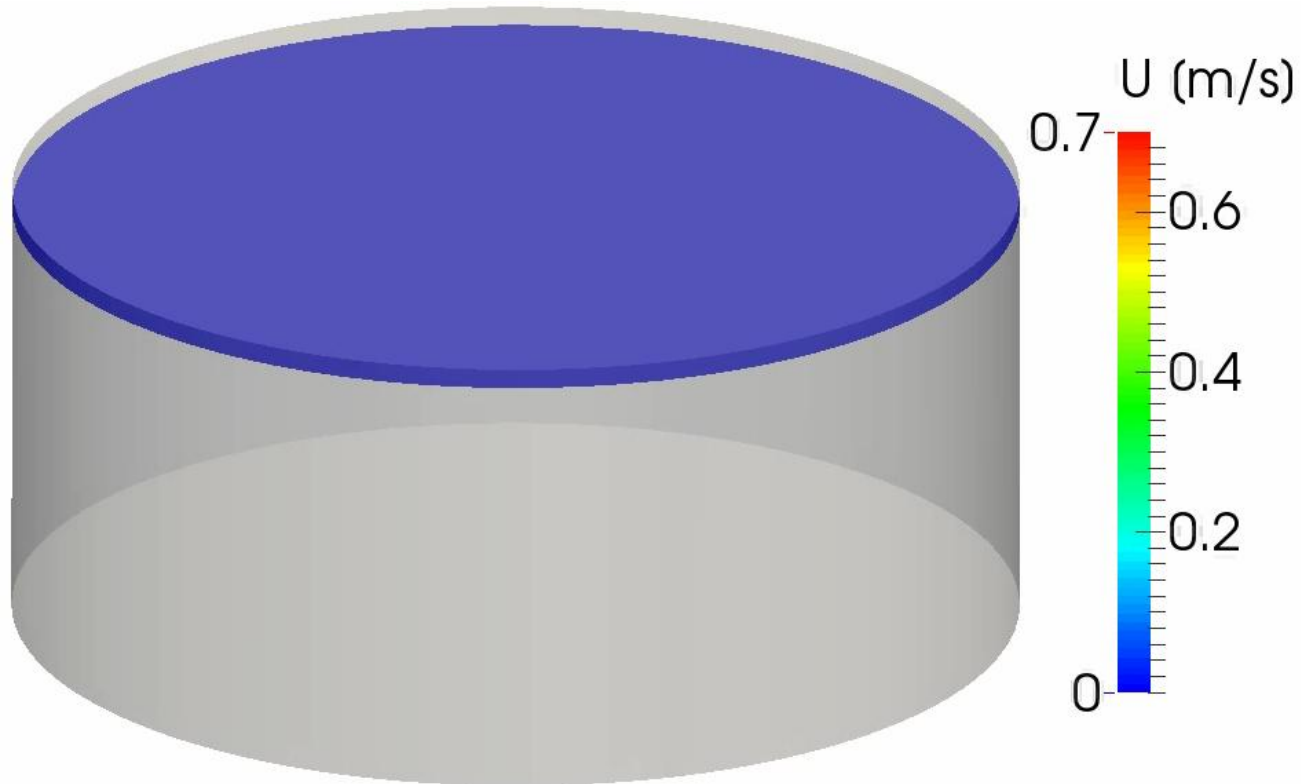
- a) Drag model impact on results quality
- b) Good agreement compared to experiment
- c) Bubble induced turbulence model
- d) Optimize conditions at inlet
- e) Change of bubble diameter

# Ladle flow

- a) Enhancement of steel homogeneity
- b) DDES model
- c) Three inlets at the bottom
- d) 490 bubbles/second
- e) Bubble diameter 4 mm
- f) Slag behavior captured by VOF

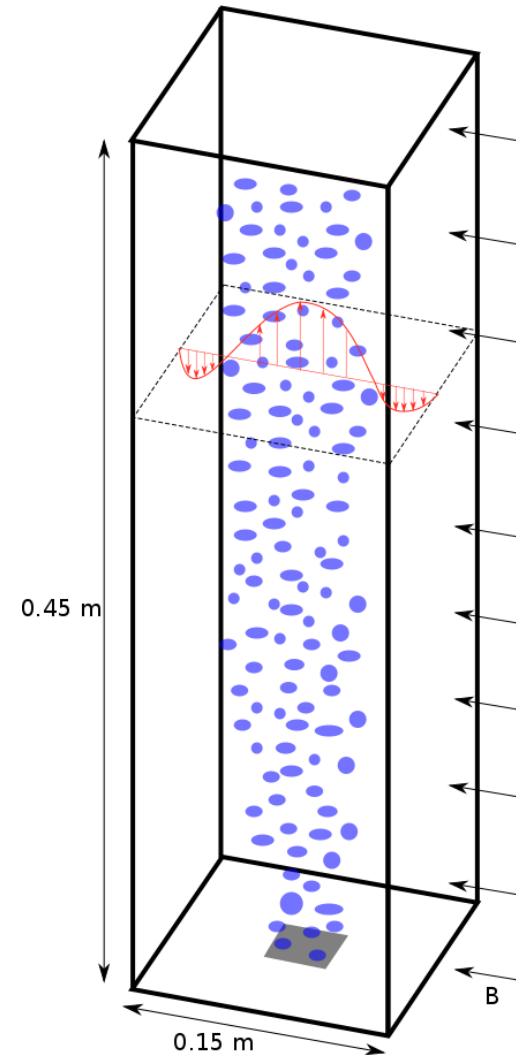


# Ladle flow



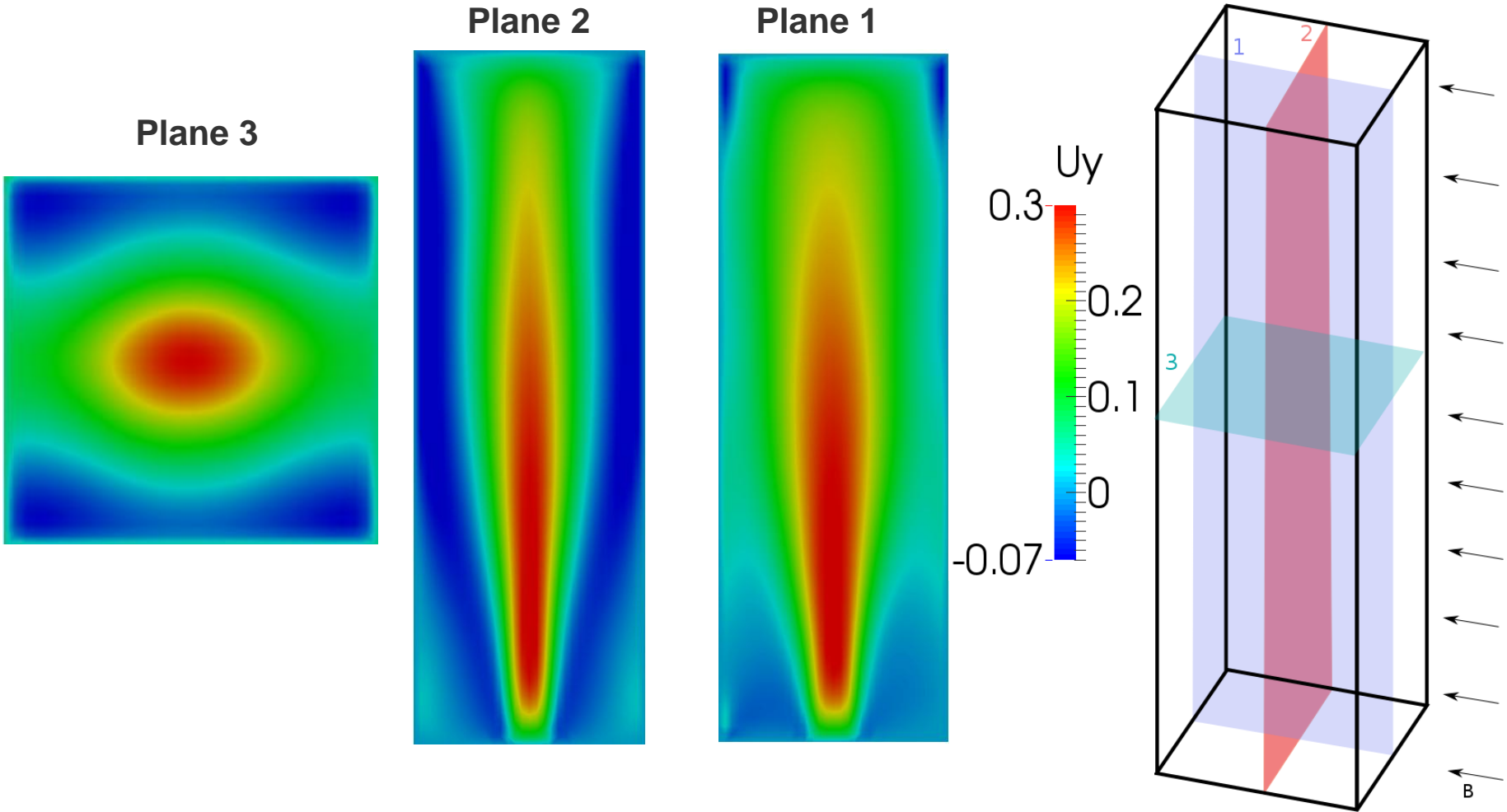
# Bubbly flow under magnetic field

- a) Argon bubbles/ melt
- b) 2300 bubbles/second
- c) Bubble diameter 4  $\mu$ m
- d) Bubbles isolated
- e) DDES model
- f)  $\underline{F}_{\text{lorentz}} = \underline{J} \wedge \underline{B}$



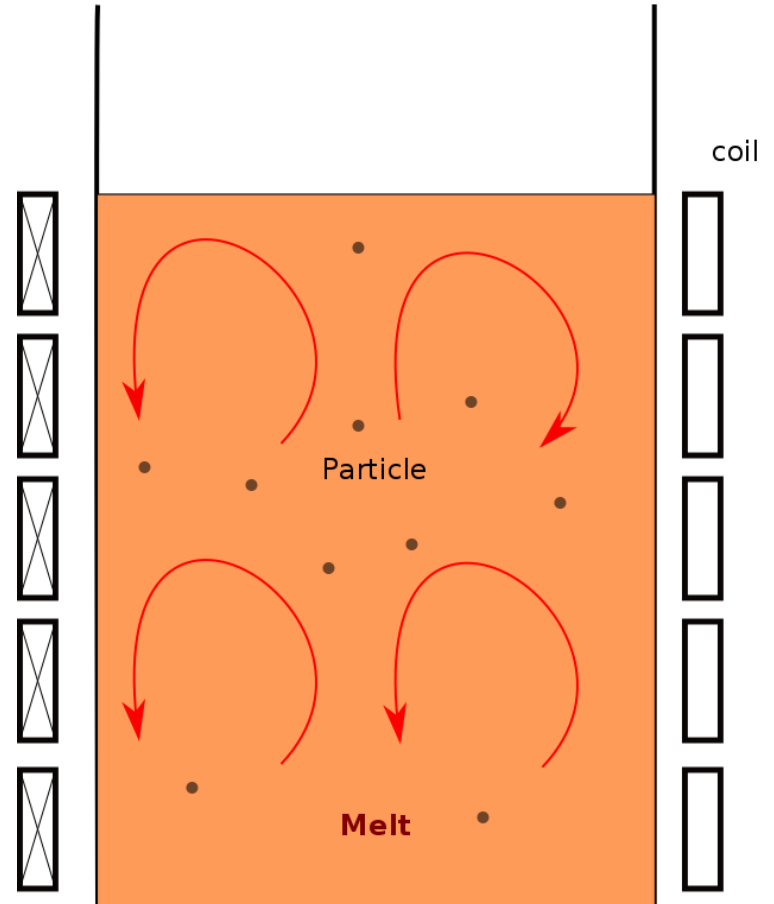
# Bubbly flow under magnetic field

## Mean vertical velocity profile of liquid metal for $B=0.05$ T



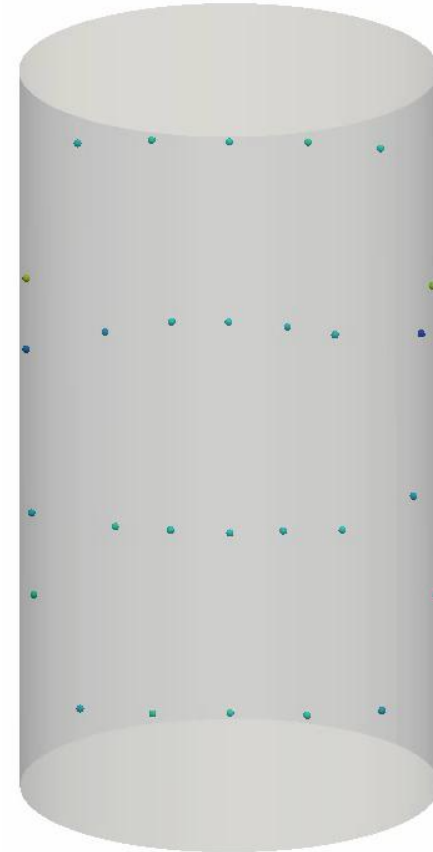
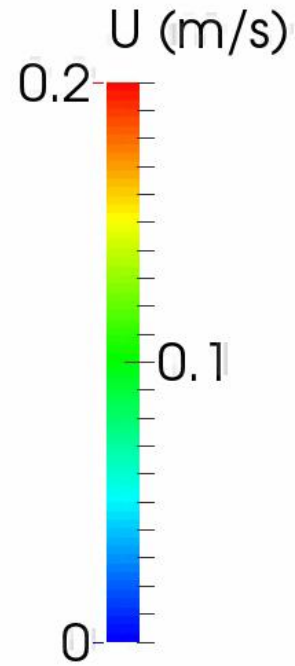
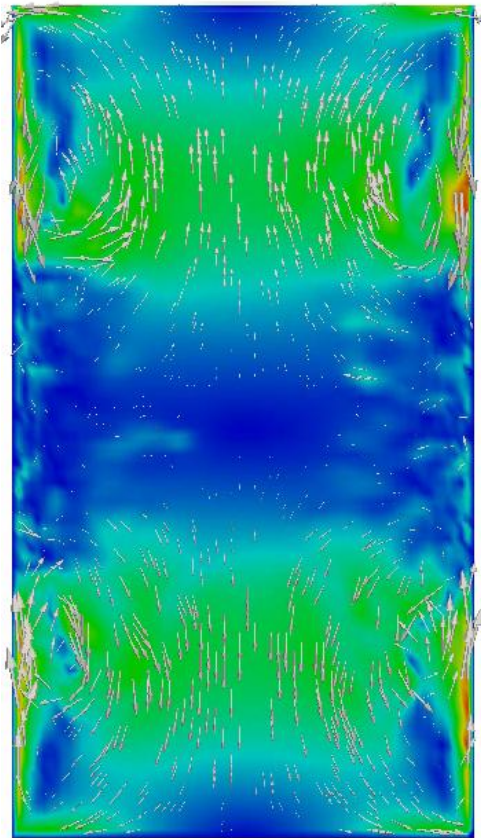
# Induction crucible furnance

- a) Alternating magnetic field
- b) Skin effect
- c) High frequency
- d) Lorentz force constant
- e) Magnetic field by MaxFEM
- f) Lorentz force interpolated
- g) Flow driven by Lorentz force
- h) Solid particles in steelmaking



# Induction crucible furnance

Slip wall

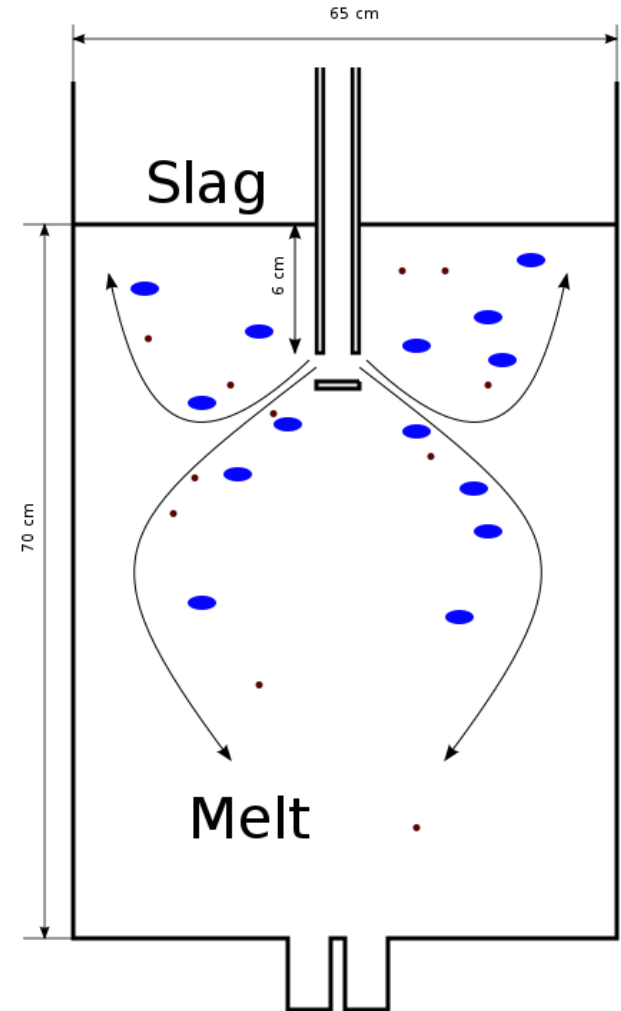


Flow field

Particles motion

# Mold flow with particles and bubbles

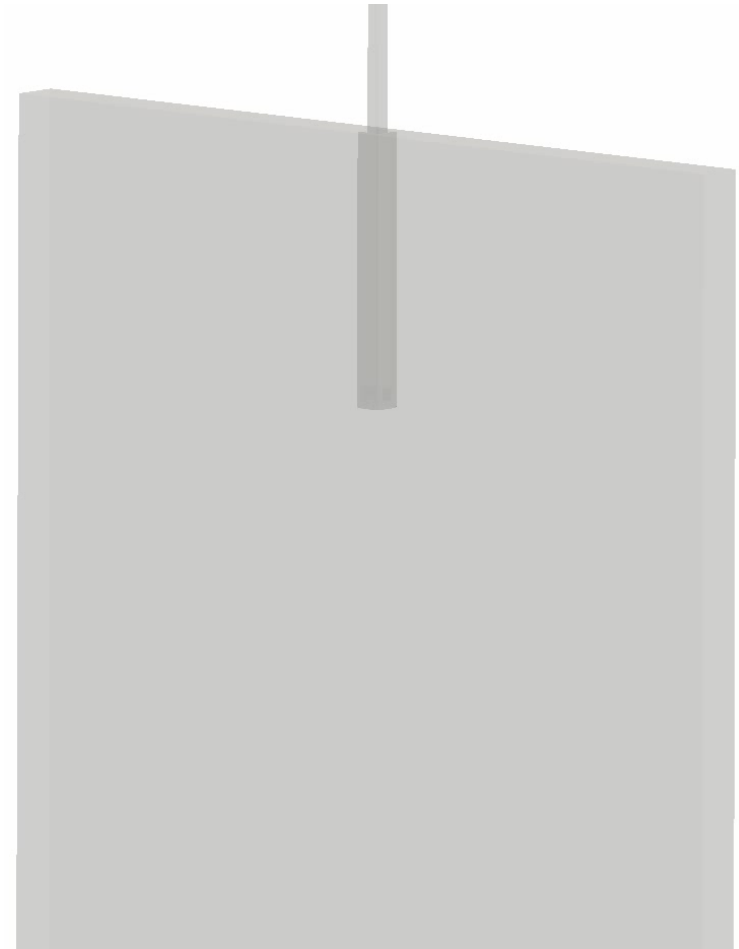
- a) 4 different phases
- b) Solid particles and bubbles at mold inlet
- c) Solid particle diameter  $20\ \mu\text{m}$
- d) Bubble diameter 3 mm
- e) Particle density  $2000\ \text{kg/m}^3$
- f) 30 particles/second
- g) 60 bubbles/second





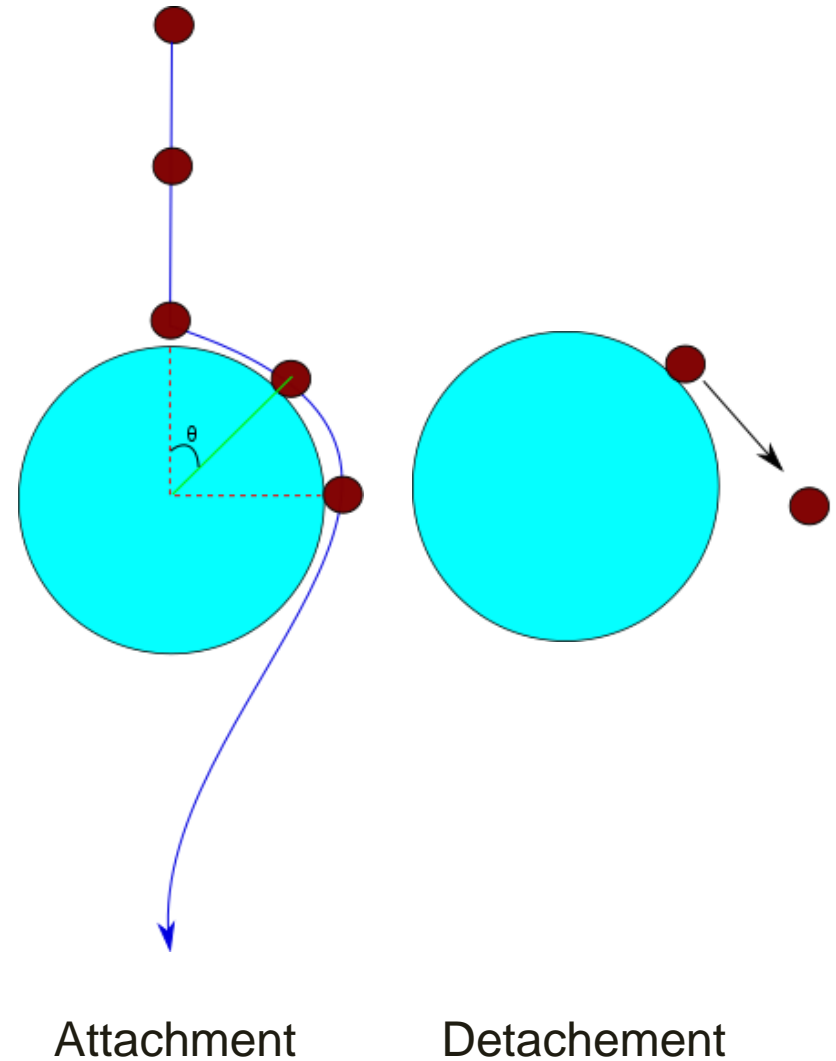
# Mold flow with particles and bubbles

- a) Solid particles: blue
- b) Bubbles: red
- c) Jet: iso-surface  $U=0.5$



# Bubble – particle attachment

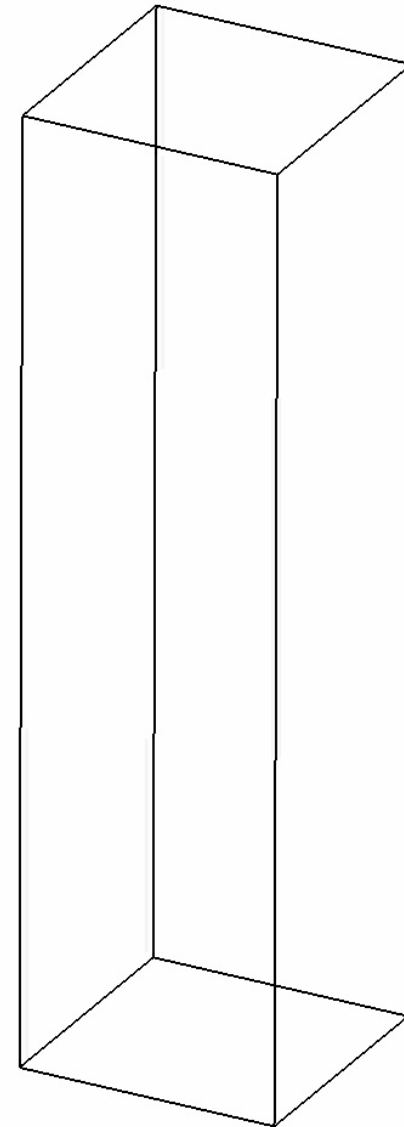
- a) Particle attaches to bubble
- b) Sliding time longer induction time
- c) Velocity, contact angle, area
- d) Detachment
- e) Collision, turbulence



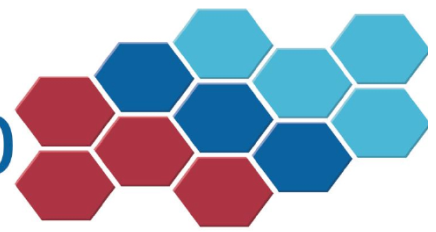
# Bubble – particle attachment

## Test case

- a) Particle diameter  $20 \mu\text{m}$
- b) Bubble diameter  $4 \text{ mm}$
- c) Simple model
- d) Particles deleted from domain
- e) Detachment not considered
- f) Model must be developed



- ❖ Discrete phase model in OpenFOAM formulated
- ❖ Model validation by means of bubble column experiment
- ❖ Ladle flow
- ❖ Bubbly flow under effect of magnetic field
- ❖ Induction crucible furnace
- ❖ Mold flow with particles and bubbles
- ❖ Bubble- particle attachment



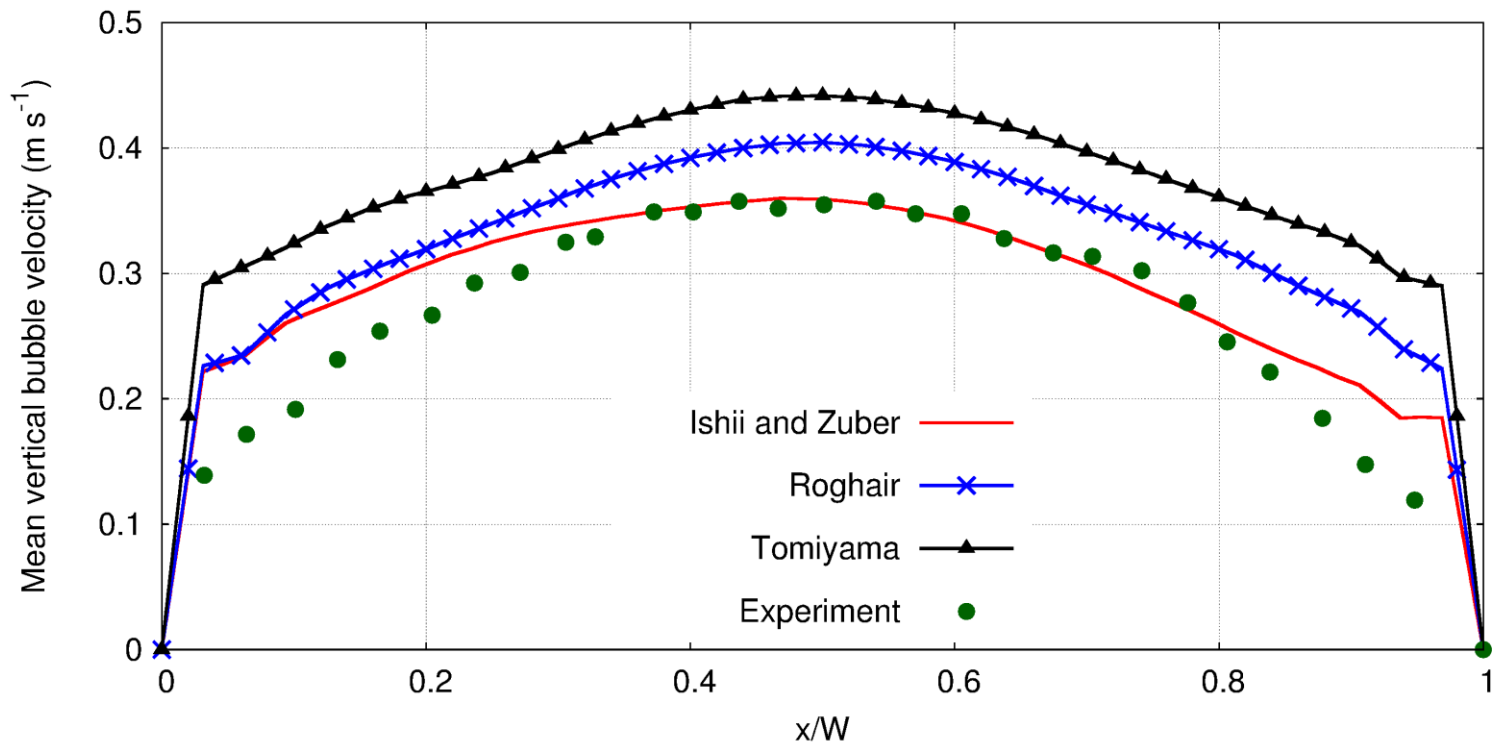
# Thanks for your Attention

## References

- [1] N. Deen, B. Hjertager, T. Solberg, In Proceedings of the 10th int. symposium on applied of laser techniques to fluid mechanics, Lisbon (Portugal) **2001**.
- [2] Tomiyama, I. Kataoka, I. Zun, T. Sakaguchi, . JSME I. J. Series B **1998**, 41,472.
- [3] M. Ishii, N. Zuber, *AIChE Journal* **1979**, 25, 843.
- [4] I. Roghair, Y. Lau, N. Deen, H.M. Slagter, M. Baltussen, M. Annaland, M. V. S., J. Kuipers. *Chem. Eng. Sci.* **2011**, 66, 3204

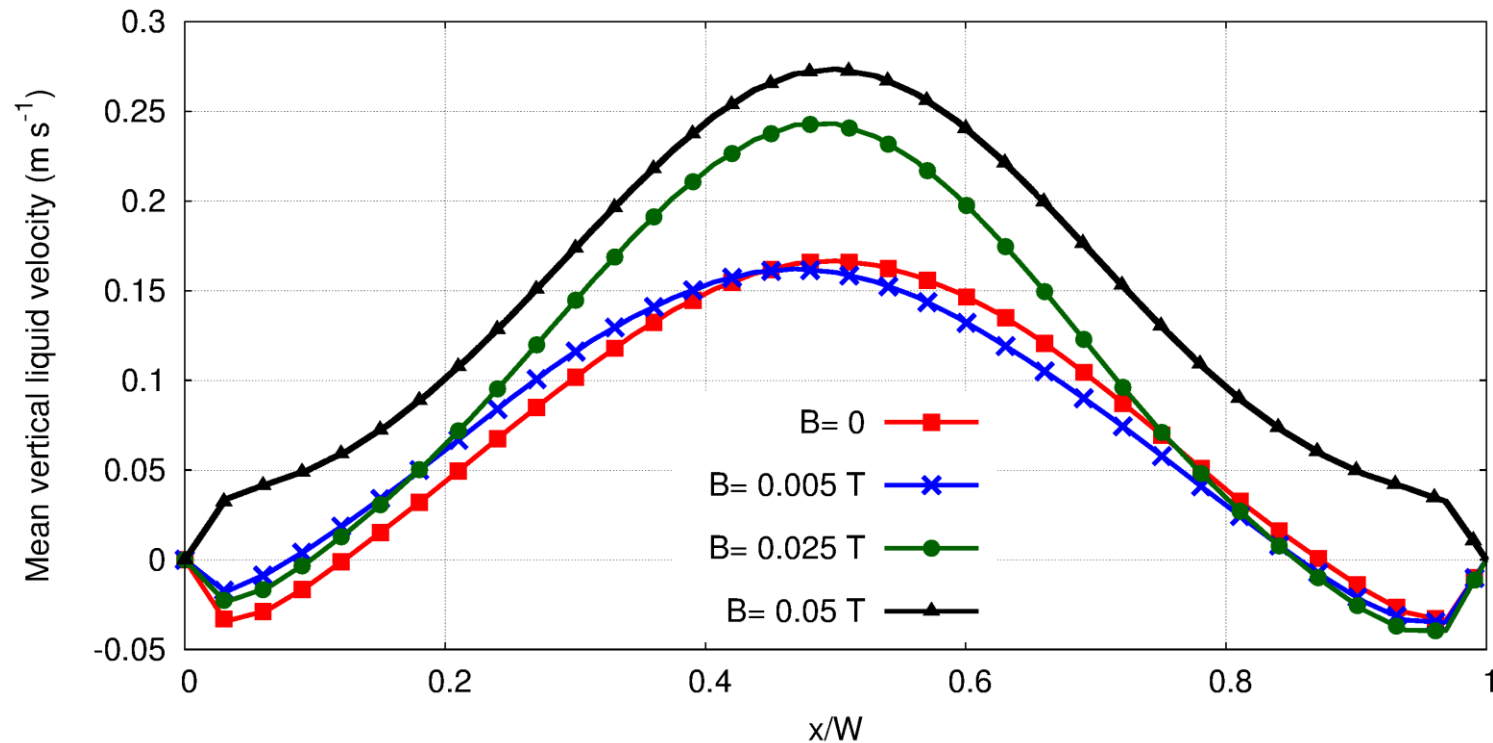
# Model Validation

## Mean vertical bubble velocity at a height of 252 mm

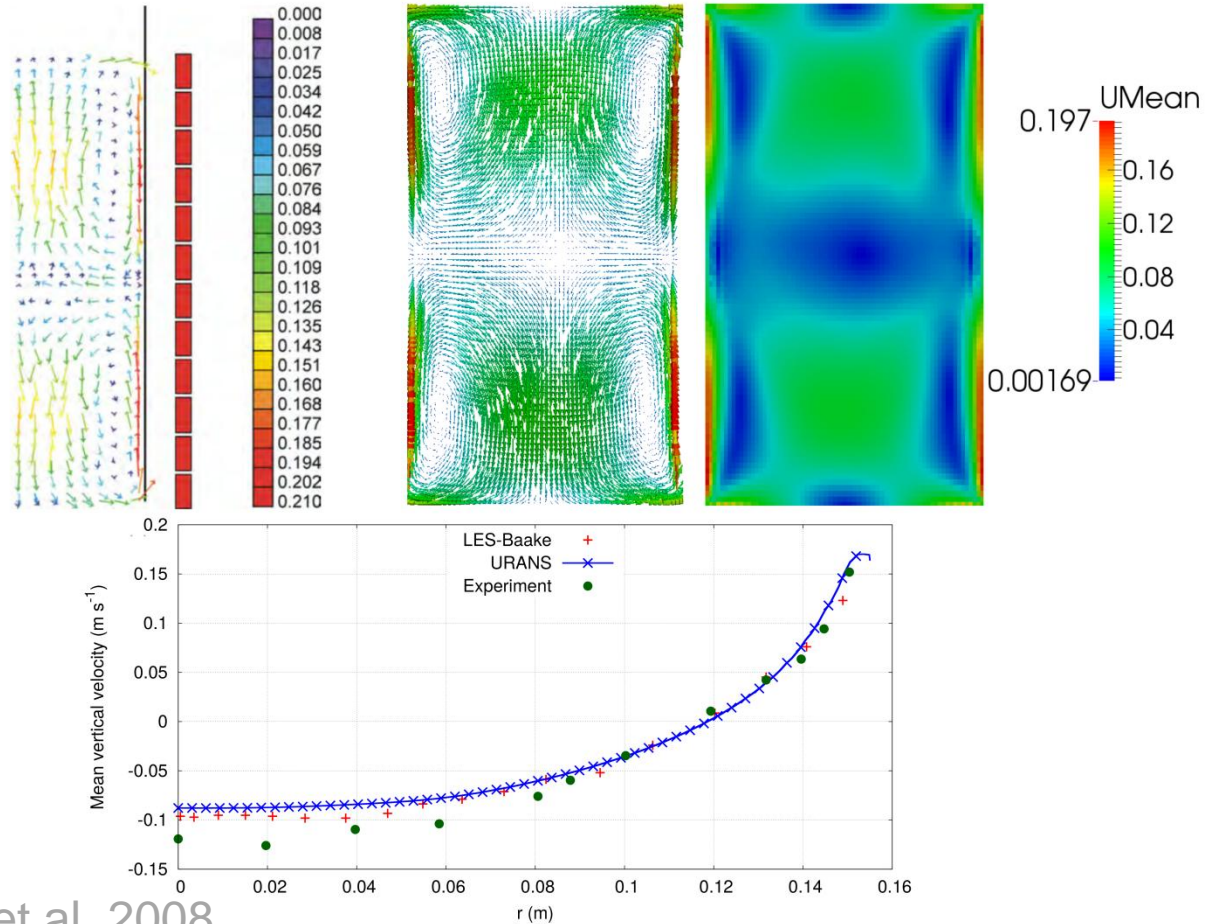


# Bubbly flow under magnetic field

## Mean vertical velocity of liquid at a height of 252 mm



# Induction crucible furnance



Kirpo et al. 2008